1. Typical Project Outline

- · Methane recovery and application from existing waste water treatment systems.
- · Methane recovery and application from new waste water treatment systems.

2. Applicability

- (1) Methane recovery from waste water treatment systems.
- (2) Application of the recovered methane for power or/and thermal generation.

3. Methodology of Emission Reduction Calculation

The emission reduction from the project activity is determined as the differences between the GHG emissions of baseline scenario (methane are emitted to atmosphere without recovery) and project scenario (recovery methane from the waste water treatment systems)¹.

Details of sources of each data in the following formulae are provided in "4. Data and Parameters for the Estimation".

$ER_{\gamma} = BE_{\gamma} - PE_{\gamma}$

ERy	: Emission reduction through the projet in year y (t-CO ₂ e/y)
BEy	: GHG emission from the baseline scenario in year y (t-CO ₂ e/y)
PEy	: GHG emission from the project scenario in year y (t-CO ₂ e/y)

(1) Calculation of Baseline Emission

The baseline emissions cover emissions from the following sources

- CO2 emissions from electricity and fossil fuels consumed in the baseline scenario
- Methane emitted to the atmosphere from waste water treatment sites in the baseline scenario
- CO₂ emissions from generation of electric power and/or thermal energy that will be replaced by electricity or thermal energy generated by the project.

$BE_{y} = BE_{EC,y} + BE_{FC,y} + BE_{ww,y} + BE_{EN,y}$

 $\begin{array}{ll} BE_{EC,y} & : CO_2 \mbox{ emissions from electricity consumed by wastewater treatment in the baseline scenario in year y (t-CO_2e/y)} \\ BE_{FC,y} & : CO_2 \mbox{ emissions from fossil fuels consumed by wastewater treatment in the baseline scenario in year y (t-CO_2e/y)} \\ BE_{ww,y} & : \mbox{ Methane emission from wastewater treatment sites in year y (t-CO_2e/y)} \\ BE_{EN,y} & : \mbox{ CO}_2 \mbox{ emissions from generation of electric power and/or thermal energy that will be replaced by electricity or thermal energy generated by the project in year (t-CO_2e/y) \end{array}$

Determination of BE_{EC,y}:

It is determined by multiplying fuel consumption with CO₂ emission factor.

 $BE_{EC,y} = EC_{BL,y} \times EF_{elec}$

¹ The target year shall be a representative year under average operation or an annual average of multiple years.

 $EC_{BL,v}$: Electricity consumption associated with wastewater treatment in the baseline scenario (MWh/y)

 EF_{elec} : CO₂ emission factor of the electricity (t-CO₂/MWh)

Determination of $BE_{FC,y}$:

It is determined as follows.

$$BE_{FC,y} = \sum_{i} (FC_{BL,i,y} \times NCV_{fuel,i} \times EF_{fuel,i} \div 10^{6})$$

 $FC_{BL,i,y}$: Amount of the fuel i consumed associated with wastewater treatment in the baseline scenario in year y (t/y) $NCV_{fuel,i}$: Net calorific value of the fuel i (TJ/Gg = TJ/kt) $EF_{fuel,i}$: CO₂ emission factor of the fuel i (kg-CO₂/TJ)

Determination of *BE_{ww,y}*:

It is determined multiplying the volume of wastewater treated in the system, the COD removed through the treatment process, CH₄ producing capacity, and global warming potential.

$BE_{ww,y} = Q_{ww,BL,y} \times COD_{ww,BL,y} \times MCF_{ww,BL} \times BO_{o,ww} \times UF_{BL} \times GWP_{CH4}$

$Q_{ww,BL,y}$: Volume of wastewater treated in wastewater treatment system in the baseline scenario in year y (m^3/y)
COD _{ww,BL,y}	: Chemical oxygen demand removed by the wastewater treatment system in the baseline scenario $(t-COD/m^3)$
MCF _{ww,BL}	: CH4 correction factor for the wastewater treatment system in the baseline scenario
BO _{o,ww}	: CH4 producing capacity of the wastewater (t-CH4/t-COD)
UF _{BL}	: Model correction factor to account for model uncertainties for baseline scenario
GWP _{CH4}	: Global Warming Potential of CH ₄ (=25 t-CO ₂ /t-CH ₄)

Determination of $BE_{EN,y}$:

It is determined by the quantity of electricity and thermal energy generated after by the project and corresponding CO₂ emission factors.

$$BE_{EN,y} = BE_{elec,y} + BE_{ther,y} = EG_{PL,y} \times EF_{elec} + HG_{PL,y}/\eta_{BL} \times EF_{fuel,k} \div 10^3$$

BE _{elec}	: Baseline emissions to generate the same amount of electricity generated by project activity in year y (t-CO ₂ /y)
BE _{heat,y}	: Baseline emissions to generated the same amount of thermal energy produced by the project activity $(t-CO_2/y)$
EG _{PJ,y}	: Amount of electricity generated by the project in year y (MWh/y)
EF _{elec}	: CO ₂ emission factor of the electricity (t-CO ₂ /MWh)
HG _{PJ,y}	: Amount of thermal energy generated by the project in year y (TJ/y)
η_{BL}	: Energy efficiency of the boiler/air heater used in the baseline scenario to generate the thermal energy.
	It will be "1" as a conservative value.

 $EF_{fuel,k}$: CO₂emission factor of the fuel k used for the boiler in the baseline scenario (kg-CO₂/TJ)

(2) Calculation of Project Emission

The project emissions equals to emissions of methane leakages from the methane recovery system.

 $PE_y = PE_{ww,y}$

 PE_v : GHG emission from the project in year y (t-CO₂e/y)

 $\mathsf{PE}_{\mathsf{ww,y}}$ \quad : Methane leakage from the methane recovery system (t-CO_2e/y)

Determination of PEwwy:

It is determined as follows.

$PE_{ww,y} = MG_{PJ,y} \times GWP_{CH4} \times EF_{CH4,def}$		
MG _{PJ,y}	: Amount of methane recovered in year y (t-CH4/y)	
GWP _{CH4}	: Global Warming Potential of CH4 (=25 t-CO ₂ /t-CH ₄)	
EF _{CH4,def}	: Methane leakage factor of the methane recovery system (t-CH4 leaked/t-CH4 produced)	

Determination of MG_{PLy}:

It is determined as follows.

$$\begin{split} MG_{PJ,y} &= Q_{ww,PJ,y} \times COD_{ww,PJ,y} \times MCF_{ww,PJ} \times BO_{o,ww} \times UF_{PJ} \\ Q_{ww,PJ,y} &: Volume of wastewater treated in the project in year y (m³/y) \\ COD_{ww,PJ,y} &: Chemical oxygen demand removed by the wastewater treatment system in the project (t-COD/m³) \\ MCF_{ww,PJ} &: CH_4 correction factor for the wastewater treatment system in the project \\ BO_{o,ww} &: CH_4 producing capacity of the wastewater (t-CH_4/t-COD) \\ UF_{PI} &: Model correction factor to account for model uncertainties for project \end{split}$$

	Description	Data Sources		
Data		For baseline emission calculation	For project emission calculation	
EC _{BL,y}	Electricity consumption associated with wastewater treatment in the baseline scenario (MWh/y)	A historical average based on the monitored/recorded values	N/A	
EF _{elec}	In the case of grid connection: CO ₂ emission factor of the grid electricity (t-CO ₂ /MWh)	A default value (Table 3, "Energy Consumption", Appendix) If there is no default value applied or if there is another appropriate value, that value may be used.	N/A	
	In the case of captive power generation or mini-grid: CO ₂ emission factor of the diesel power generation (t-CO ₂ /MWh)	A default value (Table 4, Appendix) If there is no default value applied or if there is another appropriate value, that value may be used.	N/A	
FC _{BL,i,y}	Amount of fuel i	A historical average based on the	N/A	

4. Data and Parameters for the Estimation

	L			
	consumed associated	monitored/recorded values		
	with wastewater			
	treatment in the			
	baseline scenario			
NCV	(Vyear)	An IDCC default arelys (Table 1		
NCV _{fuel,i}	Net calorific value of	An IPCC default value (Table I,		
	the fuel i $(IJ/Gg = TI/I)$	Appendix)		
	I J/Kt)	If there is no default value applied or if	N/A	
		there is another appropriate value, that		
FF		value may be used.		
L ^{IT} fuel,i	the fuel i (leg CO /TD)	An IPCC default value (Table 2,		
	the fuel I (kg-CO ₂ /IJ)	Appendix)	NI/A	
		If there is no default value applied of if	IN/A	
		there is another appropriate value, that		
FF	CO ₂ amission factor of	An IPCC default value (Table 2		
L ^{IT} fuel,k	fuel trugged for the	An IPCC default value (Table 2,		
	hailar in the baseline	Appendix)	N/Λ	
	boller in the baseline	If there is model and value applied of if	IN/A	
	scenario (kg-CO ₂ /1J)	there is another appropriate value, that		
0	Volume of wastewater	value may be used.		
≪ww,BL,y	treated in wastewater			
	treatment system in the	A monitored value	N/A	
	baseline scenario in	A monitored value		
	vear v (m^3/v)			
	Volume of wastewater			
€ww,rj,y	treated in the project in	N/A	A planned	
	vear v (m^3/v)		value	
COD _{ww.BL.v}	Chemical oxygen	A monitored value		
, ,,	demand removed by the	(Describe the measurement method		
	wastewater treatment	(chrome method or manganese method)	N/A	
	system in the baseline	in the GHG emission reduction		
	scenario (t-COD/m ³)	assessment report)		
COD _{ww,PJ,y}	Chemical oxygen	• · ·	A planned value	
	demand removed by the		(Describe the measurement method	
	wastewater treatment	N/A	(chrome method or manganese method)	
	system in the project		in the GHG emission reduction	
	(t-COD/m ³)		assessment report)	
MCF _{ww,BL}	CH ₄ correction factor			
	for the wastewater	Default value of IPCC (Table 9,	N/A	
	treatment system in the	Appendix)		
	baseline scenario			
MCF _{ww,PJ}	CH ₄ correction factor			
	for the wastewater	N/A	Default value of IPCC (Table 9,	
	treatment system in the	1011	Appendix)	
20	project			
BO _{o,ww}	CH ₄ producing capacity	0.1	25	
	of the wastewater	(Default	t value ²)	
	(t-CH4/t-COD)	(2 01441	,	
UF _{BL}	Model correction factor	0.89		
	to account for model (Default value of CDM AMS III.H.		N/A	
	uncertainties for	ver.19.0)		
UE	baseline scenario	,	1.12	
UF _{PJ}	Model correction factor	N/A		
	to account for model		(Default value of CDM AMS III.H.	

² 2019 Refinement to the 2006 IPCC Guidelines for National Greenhouse Gas Inventories, Volume 5: Waste, p.6.18

	uncertainties for project		ver.19.0)
EG _{PJ,y}	Amount of electricity generated by the projectA planned valuein year y (MWh/y)		N/A
HG _{PJ,y}	Amount of thermal energy generated by the project in year y (TJ/y)	A planned value	N/A
EF _{CH4,def}	Methane leakage factor of methane recovery system (tCH ₄ leaked/tCH ₄ produced)	N/A	0.1 (Default value: CDM Methodological Tool Project and leakage emissions from anaerobic digesters (Version 01.0.0))

5. Others

(1) Project Boundary

The project boundary is the site where the project activity is being done, where the wastes waters are treated.

(2) Leakage

Construction of power plants, replacement of facility: the indirect emissions potentially leading to leakage due to activities such as product manufacturing or materials transport in consideration of Life Cycle Assessment, LCA of disposal of waste at a solid waste disposal site. The contribution of this emission is relatively small and negligible compared with the GHG emission reduction after the project starts. Therefore, this methodology ignores the leakage provided that the technology is using equipment not transferred from another activity.

(3) Comparison with existing CDM methodologies

The logic of emission reduction calculation in the methodology is almost the same as that of the AMS-III.H (Methane recovery in wastewater treatment, Version 16). However, this methodology simplified the methodology by using default values as more as possible. For example, emissions from sludge that is not covered in the methane recovery system and waster water after treated are ignored due conservatives and simplicity. Moreover, there is no limitation for the emission reduction in the methodology like the small-scale CDM methodologies did.

Also, it is a project that collects methane generated in wastewater treatment facilities and uses it for power generation and heat supply, and there seems to be no significant difference between N₂O generated in the baseline and the project. Therefore, N₂O is ignored.

(4) Revision history

Version	Year/Month	Revisions
2.0	March 2014	• Changed the methodology name from "24. Waste water treatment (Ver 1.0)" to "Waste water
		treatment (methane recovery)"
		• Amended project emission calculation to calculate GHG emission from wastewater treated in the
		project (i.e. Methane leakage from the methane recovery system) only
		• Added default values for combined margins and operating margins of CO2 emission factors of
		electricity

3.0	September	• Prioritized the use of default values
	2019	Added instructions not to consider N ₂ O emissions
4.0	March 2023	• Deleted descriptions on treatment of sludge in the GHG emission calculation associated with
		electricity consumption under the baseline scenario.
		• Regarding the measurement of COD, added that the measurement method (chrome method or
		manganese method) should be specified in the GHG emission reduction calculation report, etc.
		• In the description of the calculation method and necessary data of baseline emissions, the words
		"before project implementation" was revised to use "the baseline scenario". The baseline scenario
		is the scenario that would have occurred in the absence of the project, such as continuation of the
		pre-project conditions.
		• Deleted the column "Ex-post" in "4. Data and Parameters Estimated and Need Monitoring":
		current version of Climate-FIT aims to quantify GHG emission reductions in the "planning
		phase").
5.0	March 2024	• Corrected the value of Model correction factor (UF) to default values of CDM methodology AMS
		III.H.
		• The source of the CH ₄ producing capacity (BO _{0,ww}) was corrected to apply IPCC 2019.
		• Removed subscript y of each parameter, which implies monitoring for each year (since
		Climate-FIT is intended to quantify GHG emission reductions in the "planning phase").